

① Clues to kinetic Regime

1.1 from solubility data

- $P_{Ai} = H_A C_{Ai}$ 
  - large  $H_A$ : slightly soluble gas (liquid film resistance controls)
  - small  $H_A$ : highly soluble gas (gas film resistance controls)
- for fast rxns occurring in the film, the solubility of the gas in the liquid can determine whether the overall process is gas phase or liquid phase control
- Consider straight mass transfer of A across the gas and liquid films:

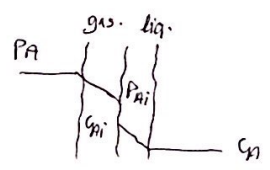
$$\frac{-1}{S} \frac{dN_A}{dt} = \frac{1}{\frac{1}{k_{Ag}} + \frac{H_A}{k_{AL}}} \Delta P_A, \Delta P_A = P_A - P_A^*, P_A^* = H_A C_A$$

1.2 From experiment

→ double CSTR

- for straight mass transfer across gas and liquid films without any rxn we have:

$$-r_A'' = \frac{-1}{S} \frac{dN_A}{dt} = k_{Ag} (P_A - P_{Ai}) = k_{AL} (C_{Ai} - C_A)$$



$P_A^* \triangleq$  equilibrium partial pressure of A in the liquid phase =  $H_A C_A$

$$\Rightarrow k_{Ag} (P_A - P_{Ai}) = k_{AL} (C_{Ai} - C_A) = K_{Ag} (P_A - P_A^*)$$

$$C_A = \frac{P_A^*}{H_A} \Rightarrow P_A^* = P_{Ai} - \frac{H_A k_{Ag}}{k_{AL}} (P_A - P_{Ai}), \frac{1}{K_{Ag}} = \frac{1}{k_{Ag}} + \frac{H_A}{k_{AL}}$$

- Advantages ✓

- we have CSTRs:  $-r_{Bl} = \frac{-1}{V_L} \frac{dN_B}{dt} = \frac{v_L (C_{B0} - C_B)}{V_L}, -r_B'' = \frac{-1}{S} \frac{dN_B}{dt} = -r_{Bl} \frac{V_L}{S} = \frac{v_L (C_{B0} - C_B)}{S}$

- Increase in gas phase agitation → ↑  $k_{Ag}$  → would increase the rate if gas phase resistance is important, otherwise no effect
- change in S &  $V_L$ 
  - If independent of  $V_L$ , but proportional to S → fast rxn regime
  - affected by both S,  $V_L$  → Intermediate
  - rate independent of S, but proportional to  $V_L$  → slow rxn

1.3 Extension to 3 phase systems

1.4 Tower Design

$$Y_A = \frac{P_A}{P_U}, X_A = \frac{C_A}{C_U}$$

• case 01 "straight mass transfer without chemical rxn"

$$G \frac{dY_A}{dh} = (-r_A'') \cdot a \Rightarrow h = \frac{G}{a} \int_{Y_{A1}}^{Y_{A2}} \frac{dY_A}{-r_A''}$$

$$\frac{dX_A}{dC_A} = \frac{C_T}{(C_T - C_A)^2} \Rightarrow \frac{G \pi d P_A}{(P - P_A)^2} = \frac{L C_T dC_A}{(C_T - C_A)^2}$$

$$h = \frac{G \pi}{a} \int_{P_{A1}}^{P_{A2}} \frac{dP_A}{k_{Ag} (P_A - P_{A1}) (P - P_A)^2} = \frac{L G}{a} \int_{C_{A1}}^{C_{A2}} \frac{dC_A}{C_{A1} k_{AL} (C_{A1} - C_A) (C_T - C_A)^2}$$

- special case: dilute system

• case 02

